

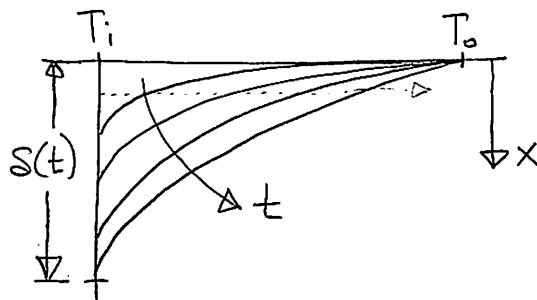
Two Dimensional Conduction (x, t) $T(x, t)$, $\dot{Q}''' = 0$, $V = 0$, $k = \text{constant}$, $\alpha = \text{constant}$

We derived previously that:

$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} + \frac{\dot{Q}'''}{k} = \frac{1}{\alpha} \frac{\partial T}{\partial t}$$

$$\frac{\partial^2 T}{\partial x^2} = \frac{1}{\alpha} \frac{\partial T}{\partial t}$$

Here we need 2 boundary conditions and 1 initial condition



T_o = hot body temperature
 T_i = initial temperature

So our governing PDE is: $\theta = \frac{T - T_o}{T_i - T_o}$

$$\frac{\partial^2 \theta}{\partial x^2} = \frac{1}{\alpha} \frac{\partial \theta}{\partial t}$$

$$x = 0, \theta = 0$$

$$x \rightarrow \infty, \theta = 1$$

$$t = 0, \theta = 1$$

} Separation of variables won't work since the medium is infinite.

The only way to solve this is to look for a similarity variable, that relates x, t . One that works and is convenient is:

$$\eta = \frac{x}{f(t)}, \text{ so } \theta(\eta), f(t) = \text{function of time}$$

$$\frac{\partial \theta}{\partial x} = \frac{\partial \theta}{\partial \eta} \frac{\partial \eta}{\partial x} = \frac{1}{f} \frac{\partial \theta}{\partial \eta}$$

} Note, if you use Buckingham PI theorem you will get $\pi_1 = \theta$, $\pi_2 = \frac{x}{\sqrt{\alpha t}}$.

$$\frac{\partial^2 \theta}{\partial x^2} = \frac{\partial}{\partial x} \left(\frac{\partial \theta}{\partial x} \right) = \frac{1}{f} \frac{\partial}{\partial x} \left(\frac{\partial \theta}{\partial \eta} \right) = \frac{1}{f} \frac{2}{\partial \eta} \left(\frac{\partial \theta}{\partial \eta} \right) \frac{\partial \eta}{\partial x} = \frac{1}{f^2} \frac{\partial^2 \theta}{\partial \eta^2}$$

$$\frac{\partial \Theta}{\partial t} = \frac{\partial \Theta}{\partial \eta} \cdot \frac{\partial \eta}{\partial t} = -\frac{\partial \Theta}{\partial \eta} \cdot x \cdot \frac{f'}{f^2} = -\eta \frac{\partial \Theta}{\partial \eta} \frac{f'}{f}$$

Now if we back substitute into our PDE

$$\frac{1}{f^2} \frac{\partial^2 \Theta}{\partial \eta^2} + \frac{f'}{f} \eta \cdot \frac{\partial \Theta}{\partial \eta} = 0$$

$$\frac{\partial^2 \Theta}{\partial \eta^2} + \underbrace{\left(\frac{f \cdot f'}{\alpha} \right)}_{\text{Let this term equal to a constant}} \eta \frac{\partial \Theta}{\partial \eta} = 0$$

$$\frac{ff'}{\alpha} = 2 \quad (\text{can choose any arbitrary number})$$

$$\frac{f \partial f}{\partial t} = 2\alpha \Rightarrow \int f \partial f = \int 2\alpha \partial t$$

$$\frac{f^2}{2} = 2\alpha t$$

$$f = 2\sqrt{\alpha t}$$

$$\frac{ff'}{\alpha} \cdot \eta = 2\eta$$

$$\eta = \frac{x}{2\sqrt{\alpha t}} \Rightarrow \frac{\partial^2 \Theta}{\partial \eta^2} + 2\eta \frac{\partial \Theta}{\partial \eta} = 0 \Rightarrow \text{ODE}$$

Our new B.C.'s become: $\eta = 0, \Theta = 0$ } Turned 2BC's & IC
 $\eta \rightarrow \infty, \Theta = 1$ } into 2BC's only

Rewriting our ODE

$$\frac{\Theta''}{\Theta'} = -2\eta$$

$$\Rightarrow \boxed{\frac{d}{dx} \ln(\Theta') = \frac{1}{\Theta'} \cdot \frac{d}{dx} (\Theta')}$$

$$\text{Rewrite as: } \frac{2}{2\eta} (\ln \Theta')$$

$$\frac{2}{2\eta} \ln(\Theta') = -2\eta$$

$$\int 2 \ln(\Theta') = \int -2\eta \partial \eta$$

$$\ln(\Theta') = -\frac{2\eta^2}{2} + C = -\eta^2 + C \quad (\text{Take } \ln(\dots) \text{ of both sides})$$

$$\Theta' = C e^{-\eta^2}$$

Integrating again,

$$\Theta = C \int_0^n e^{-n^2} dn + C_2$$

We know $\Theta(n=0) = 0 \Rightarrow C_2 = 0$
 $\Theta(n \rightarrow \infty) = 1$

$$1 = C \int_0^\infty e^{-n^2} dn \quad (\text{Gaussian integral})$$

$$I_0 = \frac{\sqrt{\pi}}{2} \Rightarrow C = \frac{2}{\sqrt{\pi}}$$

$$\therefore \Theta = \frac{T - T_0}{T_i - T_0} = \frac{2}{\sqrt{\pi}} \int_0^n e^{-n^2} dn = \operatorname{erf}\left(\frac{x}{2\sqrt{\alpha t}}\right)$$

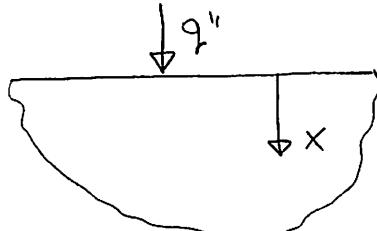
This integral cannot be solved analytically. Must be done numerically.

For the error function, see Table B4, pg 924 in Mills. Also: $1 - \operatorname{erf}(n) = \operatorname{erfc}(n)$

error function
tabulated results

complimentary error function.

So what about heat transfer during transient conduction?



$$q''|_{x=0} = -k \frac{\partial T}{\partial x}|_{x=0} \Rightarrow \text{let } \Theta = \frac{T - T_0}{T_i - T_0}, \quad d\Theta = \frac{1}{T_i - T_0} dT$$

$$= -k(T_i - T_0) \frac{\partial \Theta}{\partial x}|_{x=0} = k \underbrace{(T_0 - T_i)}_{\Delta T} \underbrace{\frac{\partial \Theta}{\partial x}}_{\frac{1}{2\sqrt{\alpha t}}} \left(\frac{\partial \Theta}{\partial n} \right)|_{x=0}$$

$$q'' = \frac{k \Delta T}{\sqrt{\pi \alpha t}}$$

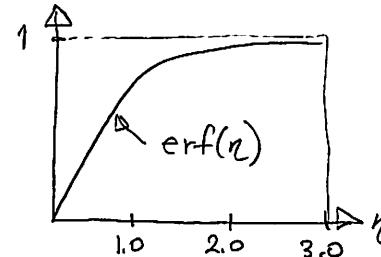
$$\alpha = \frac{k}{\rho C}$$

$$\frac{1}{2\sqrt{\alpha t}} \frac{2}{\sqrt{\pi}}$$

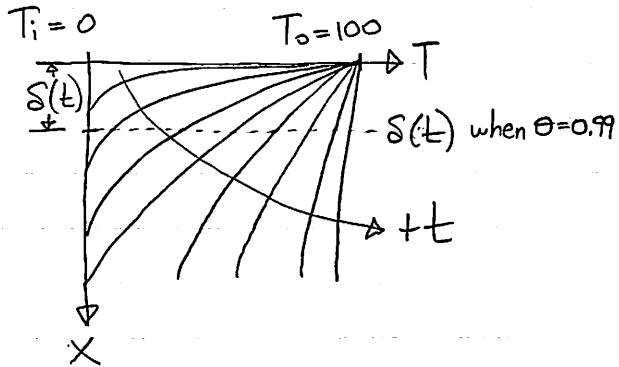
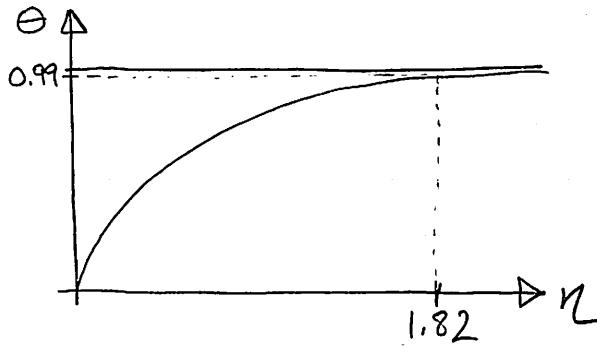
\Rightarrow Thermal diffusivity

Note, to get total energy transferred, you need to integrate q'' .

Aside: Error function



Lets analyze our solution: $\Theta = \frac{T - T_i}{T_o - T_i}$



$$\frac{S}{2\sqrt{\alpha t}} = 1.82 \Rightarrow S(t) = 3.04\sqrt{\alpha t} \Rightarrow \text{Thermal penetration depth}$$

Lets look at some other cases:

- ① Specified surface heat flux, $q'' = \text{constant}$

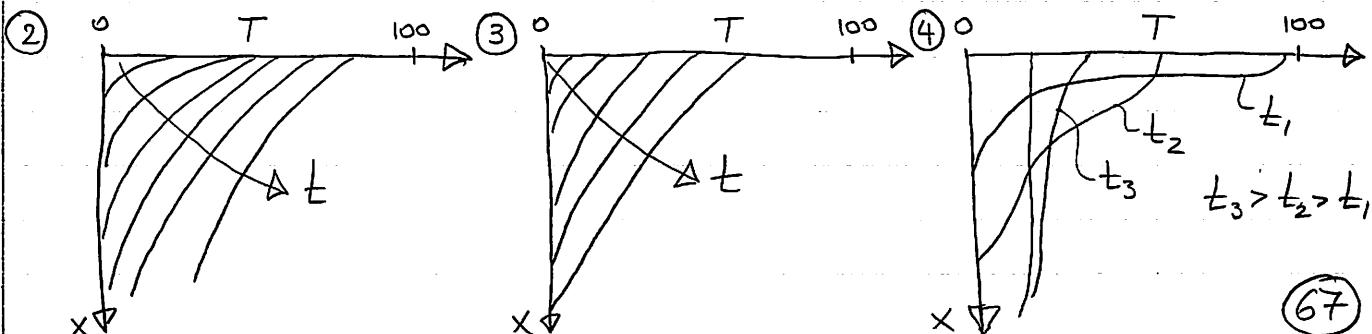
$$T(x,t) - T_i = \frac{q''}{k} \left[\frac{\sqrt{4\alpha t}}{\pi} e^{-\frac{x^2}{4\alpha t}} - x \operatorname{erfc}\left(\frac{x}{2\sqrt{\alpha t}}\right) \right]$$

- ② Convection on the surface, $q'' = h(T_\infty - T(0,t))$

$$\frac{T(x,t) - T_i}{T_\infty - T_i} = \operatorname{erfc}\left(\frac{x}{2\sqrt{\alpha t}}\right) - e^{\left(\frac{hx}{k} + \frac{h^2 \alpha t}{k^2}\right)} \cdot \operatorname{erfc}\left(\frac{x}{2\sqrt{\alpha t}} + \frac{h\sqrt{\alpha t}}{k}\right)$$

- ③ Energy pulse at surface, $e_s = \text{constant}$ $\left[\frac{\text{J}}{\text{m}^2}\right]$ @ $t=0$
Like a laser pulse, no losses, all heat goes into the solid

$$T(x,t) - T_i = \frac{e_s}{k\sqrt{\pi t/\alpha}} e^{-\frac{x^2}{4\alpha t}}$$



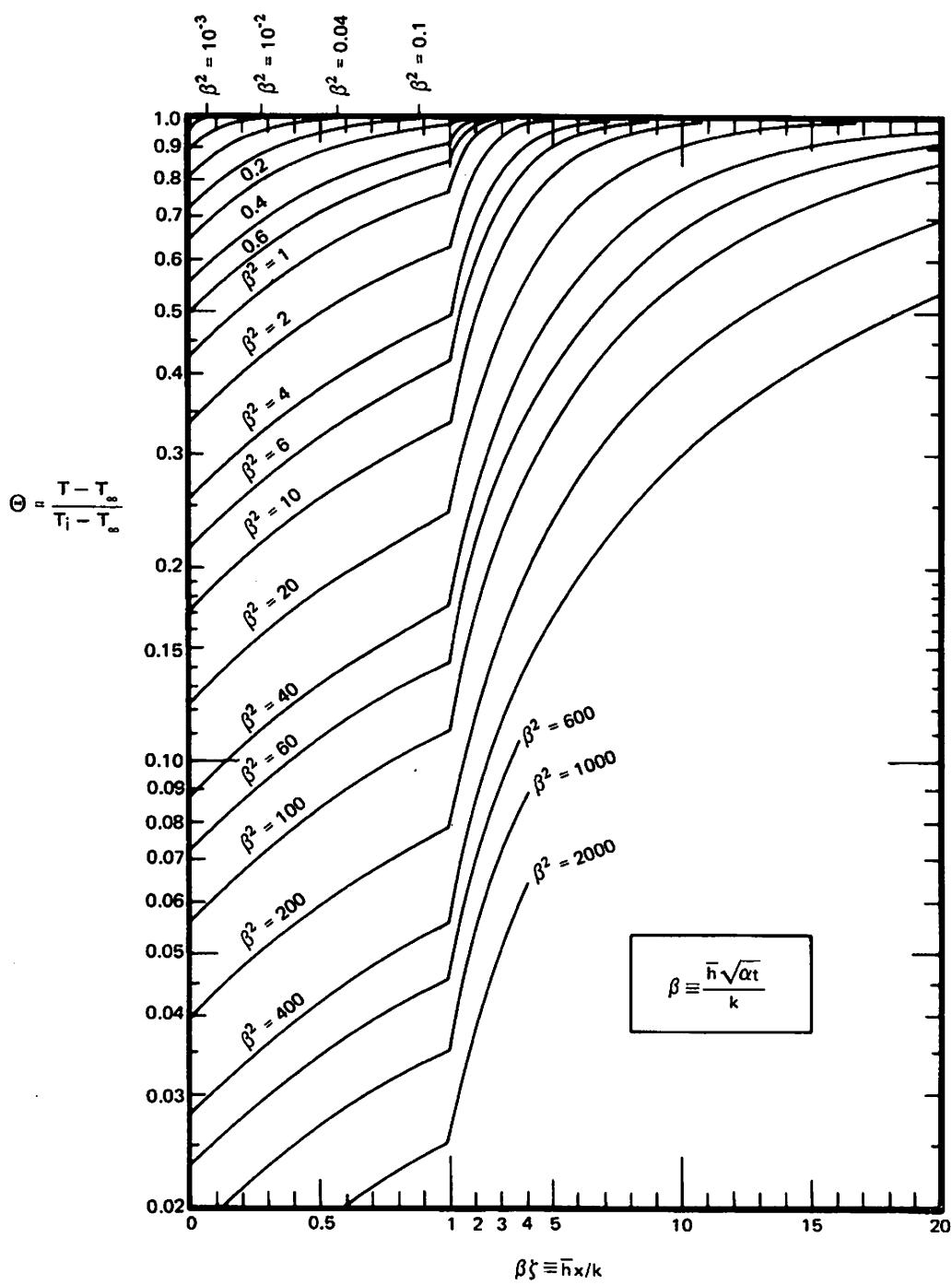
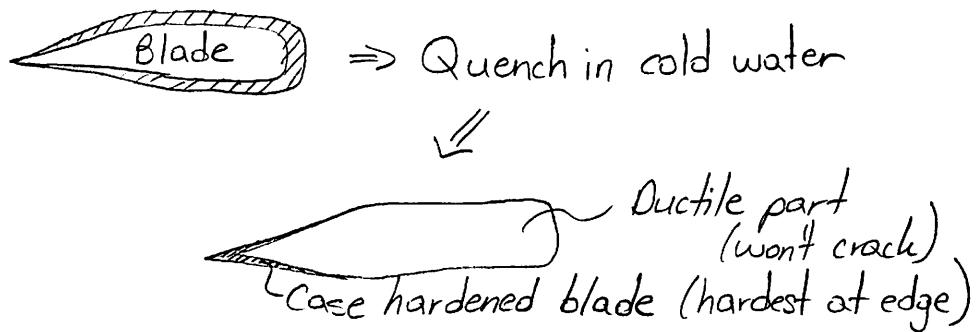


Figure 5.16 The cooling of a semi-infinite region by an environment at T_∞ , through a heat transfer coefficient, \bar{h} .

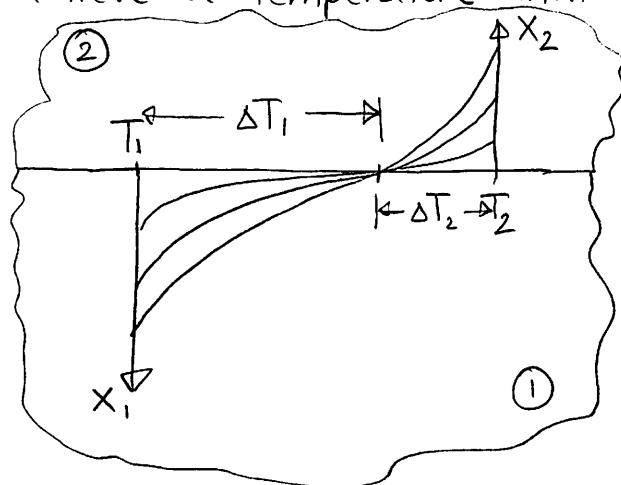
From: J.H. Lienhard IV and J.H. Lienhard V. *A Heat Transfer Textbook*, Phlogiston Press, Cambridge, MA, 3rd edition, 2008. Used by permission.

Application: Samurai in Japan used to make their swords with transient heat conduction in mind. They would coat the blade with clay sheath & quench



Contact of Two Semi-Infinite Solids

Two bodies at T_1 & T_2 brought into contact, they instantly achieve a temperature that is constant at their interface



Note, $T_{\text{interface}} \neq f(t) = \text{constant}$

$T_{\text{interface}}$ will develop very quickly after the two bodies touch, & remain the same.

Applying an energy balance, $\Delta T = T_1 - T_2$

$$q'' = \frac{k \Delta T}{\sqrt{\pi} a t} = \frac{(k \rho c)^{1/2}}{\sqrt{\pi}} \cdot \frac{\Delta T}{\sqrt{t}}$$

$$q''_1 = q''_2 \Rightarrow \frac{(k_1 \rho_1 c_1)^{1/2}}{\sqrt{\pi}} \cdot \frac{\Delta T_1}{\sqrt{t}} = \frac{(k_2 \rho_2 c_2)^{1/2}}{\sqrt{\pi}} \cdot \frac{\Delta T_2}{\sqrt{t}}$$

$$(k_1 \rho_1 c_1)^{1/2} \Delta T_1 = (k_2 \rho_2 c_2)^{1/2} \Delta T_2 \quad ①$$

$$\Delta T_1 + \Delta T_2 = \Delta T \quad ②$$

Back substituting ② into ①

$$\Delta T_2 = \frac{(kpc)_1^{1/2}}{(kpc)_2^{1/2}} \cdot \Delta T_1$$

$$\Delta T = \left(1 + \sqrt{\frac{(kpc)_1}{(kpc)_2}} \right) \Delta T_1$$

$$\Delta T_1 = \frac{\Delta T}{1 + \sqrt{\frac{(kpc)_1}{(kpc)_2}}} = \frac{(kpc)_2^{1/2} \cdot \Delta T}{(kpc)_2^{1/2} + (kpc)_1^{1/2}}$$

$$q''_{x=0} = \frac{(kpc)_1^{1/2} (kpc)_2^{1/2}}{(kpc)_1^{1/2} + (kpc)_2^{1/2}} \cdot \frac{\Delta T}{\sqrt{\pi E}}$$

$\neq f(t)$, $\therefore T_{\text{interface}} = \text{const.}$

\Rightarrow Heat flux between the two contacting bodies

Note, this is fundamentally why when you touch certain objects in a room, they feel "colder" than others, even though they are at the same temperature.

Example | Touching a brass & wooden doorknob.

Brass: $k_1 = 109 \text{ W/m}\cdot\text{K}$

$\rho_1 = 8730 \text{ kg/m}^3$

$C_1 = 380 \text{ J/kg}\cdot\text{K}$

$$(k_1 \rho_1 C_1)^{1/2} = 19016$$

Wood: $k_2 = 0.17 \text{ W/m}\cdot\text{K}$ (Oak)

$\rho_2 = 750 \text{ kg/m}^3$

$C_2 = 1700 \text{ J/kg}\cdot\text{K}$

$$(k_2 \rho_2 C_2)^{1/2} = 466$$

Let's say $\Delta T = T_{\text{body}} - T_{\text{room}} \approx 20^\circ\text{C}$

Now we need human flesh properties.

Human Hand: $k_3 \approx 0.6 \text{ W/m}\cdot\text{K}$

$\rho_3 \approx 1000 \text{ kg/m}^3$

$C_3 \approx 4190 \text{ J/kg}\cdot\text{K}$

$$(k_3 \rho_3 C_3)^{1/2} = 1586$$

Case 1: Brass Doorknob

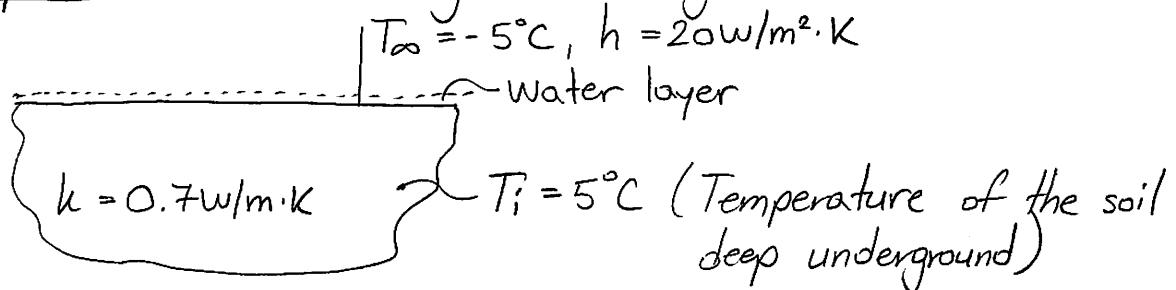
$$q''_{3+1} = \frac{(19016)(1586)}{(19016) + (1586)} \cdot \frac{\Delta T}{\sqrt{\pi E}} = 1463 \frac{\Delta T}{\sqrt{\pi E}}$$

Case 2: Wooden Doorknob

$$\frac{q''_{3 \rightarrow 2}}{q''_{3 \rightarrow 1}} = \frac{(466)(1586)}{466+1586} \cdot \frac{\Delta T}{\sqrt{\pi E'}} = 360 \frac{\Delta T}{\sqrt{\pi E'}}$$

We see that: $\frac{q''_{3 \rightarrow 1}}{q''_{3 \rightarrow 2}} \approx 4.1 \Rightarrow$ The brass doorknob will feel about 4 times "colder"

Your body senses heat by monitoring heat flux, not temperature, so the feeling of relative coldness depends on how fast you lose heat.

Example | Water freezing on the ground

$$\Theta = \frac{T - T_\infty}{T_i - T_\infty} = \frac{0^\circ\text{C} - (-5^\circ\text{C})}{5^\circ\text{C} - (-5^\circ\text{C})} = 0.5 \quad , \text{ note } T=0^\circ\text{C because of water freezing temp.}$$

$x = 0$ (top of soil)

Using our chart: 5.16 from Lienhard & Lienhard, 2008

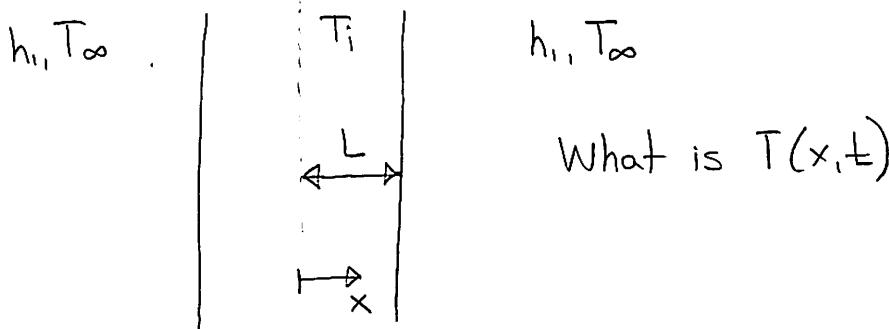
$$\beta^2 = 0.6 = \left(\frac{h}{k}\right)^2 \alpha t \Rightarrow \boxed{t = 24 \text{ minutes}}$$

Therefore, ice will freeze in ≈ 24 minutes on the ground.

Transient Heat Conduction in Finite Bodies

Previously, we covered lumped capacitance : $T = f(t) \neq f(x)$
 and transient heat conduction in infinite media : $0 \leq x \leq \infty$
 What about finite bodies : $0 \leq x \leq L$?

Plane wall problem: Wall initially at T_i placed in medium at T_∞ & h_i on outside.



Writing out our heat equation:

$$\frac{\partial^2 T}{\partial x^2} = \frac{1}{\alpha} \frac{\partial T}{\partial t}$$

$$T(x, t=0) = T_i \quad (\text{initial condition})$$

$$\left. \frac{\partial T}{\partial x} \right|_{x=0} = 0 \quad (1^{\text{st}} \text{ B.C.})$$

$$-k \left. \frac{\partial T}{\partial x} \right|_{x=L} = h(T - T_\infty) \quad (2^{\text{nd}} \text{ B.C.})$$

To make things simpler, its helpfull to non-dimensionalize

Let $\bar{x} = \frac{x}{L}$, $\partial \bar{x} = \frac{1}{L} \partial x$ (Dimensionless distance from center)

$$\Theta = \frac{T - T_\infty}{T_i - T_\infty}, \quad \partial \Theta = \frac{1}{T_i - T_\infty} \cdot \partial T \quad (\text{Dimensionless temperature})$$

What about dimensionless time τ ?

$$\frac{\partial T}{\partial x} = \frac{(T_i - T_\infty)}{L} \frac{\partial \Theta}{\partial \bar{x}}$$

$$\frac{\partial^2 T}{\partial x^2} = \frac{(T_i - T_\infty)}{L^2} \frac{\partial^2 \Theta}{\partial \bar{x}^2}$$

$$\frac{\partial T}{\partial t} = (T_i - T_\infty) \frac{\partial \Theta}{\partial \tau}$$

Back substituting

$$\frac{(T_i - T_\infty)}{L^2} \frac{\partial^2 \Theta}{\partial \bar{x}^2} = (T_i - T_\infty) \frac{\partial \Theta}{\partial t} \cdot \frac{1}{\alpha}$$

$$\frac{\partial^2 \Theta}{\partial \bar{x}^2} = \frac{L^2}{\alpha} \frac{\partial \Theta}{\partial t}$$

So this helps us solve for Θ : $\int \partial t = \int \frac{L^2}{\alpha} \partial \Theta$

$$\Theta = \frac{\alpha t}{L^2} \Rightarrow \text{Fourier number}$$

Aside: Fourier # simplified

$$F_o = \frac{\alpha t}{L^2} = \frac{k t}{\rho c L^2} \frac{\Delta T}{\Delta T} = \frac{\left(k \frac{\Delta T}{L} \right)}{\left(\frac{\rho c \Delta T L}{t} \right)} = \frac{q'' \text{ cond}}{q'' \text{ stored}}$$

$$\Theta = F_o = \frac{\alpha t}{L^2} = \frac{\text{diffusive heat conduction rate}}{\text{heat storage rate (transient)}} = \text{dimensionless time in h.t. problems.}$$

Now if we non-dimensionalize our second boundary condition

$$-k \frac{\partial T}{\partial x} \Big|_{x=L} = h(T - T_\infty)$$

$$-k \frac{(T_i - T_\infty)}{L} \frac{\partial \Theta}{\partial \bar{x}} \Big|_{x=1} = h \Theta (T_i - T_\infty)$$

We can rewrite this as:

$$\frac{\partial \Theta(1, \Theta)}{\partial \bar{x}} = - \underbrace{\frac{hL}{k}}_{-\beta_{i,L}} \Theta(1, \Theta)$$

$$-\beta_{i,L} \Rightarrow \text{Biot number} = \text{dimensionless h.t.c.} \\ = \frac{\text{conduction resistance}}{\text{convection resistance}}$$

Our other B.C. & I.C. are:

$$\frac{\partial \Theta(0, \Theta)}{\partial \bar{x}} = 0$$

$$\Theta(\bar{x}, 0) = 1$$

Note we've taken the problem from: $T(x, t) = f(x, L, t, \alpha, h, T_\infty, T_i)$

$$\text{to: } \Theta = f(\bar{x}, \beta_{i,L}, F_o) \Rightarrow \text{Very Powerful!}$$

To solve, we need to use separation of variables:

$$\Theta(\bar{x}, \bar{c}) = F(\bar{x}) \cdot G(\bar{c})$$

Back substituting & dividing by FG

$$\underbrace{\frac{1}{F} \frac{\partial^2 F}{\partial \bar{x}^2}}_{f(\bar{x}) \text{ only}} = \underbrace{\frac{1}{G} \frac{\partial G}{\partial \bar{c}}}_{f(\bar{c}) \text{ only}} = \text{Constant}$$

(The only valid solution)
 $\neq 0$ since that says no time dependence. $G \neq f(\bar{c})$.
 $(\bar{x}, \bar{c} \text{ can be varied independently})$

We will assume a solution of the form $-\lambda^2$

$$\frac{\partial^2 F}{\partial \bar{x}^2} + \lambda^2 F = 0 \quad ①$$

$$\frac{\partial G}{\partial \bar{c}} + \lambda^2 G = 0 \quad ②$$

Solving ① first: $\lambda'^2 + \lambda^2 = 0$
 $\lambda' = \pm \sqrt{-1} \lambda = \lambda i$

So our solution becomes:

$$F = C_1 e^{i\lambda \bar{x}} + C_2 e^{-i\lambda \bar{x}} \Rightarrow \text{since } \sin x = \frac{e^{ix} - e^{-ix}}{2i}$$

Can rewrite our solution as:

$$\cos x = \frac{e^{ix} + e^{-ix}}{2}$$

$$F = C_1 \cos(\lambda \bar{x}) + C_2 \sin(\lambda \bar{x})$$

For G:

$$\lambda'^2 + \lambda^2 = 0 \Rightarrow \lambda' = -\lambda^2$$

$$G = C_3 e^{-\lambda^2 \bar{c}}$$

Combining our solution, we obtain:

$$\Theta = F \cdot G = C_3 e^{-\lambda^2 \bar{c}} (C_1 \cos(\lambda \bar{x}) + C_2 \sin(\lambda \bar{x})) = e^{-\lambda^2 \bar{c}} [A \cos(\lambda \bar{x}) + B \sin(\lambda \bar{x})] \quad (73)$$

Applying our B.C.'s:

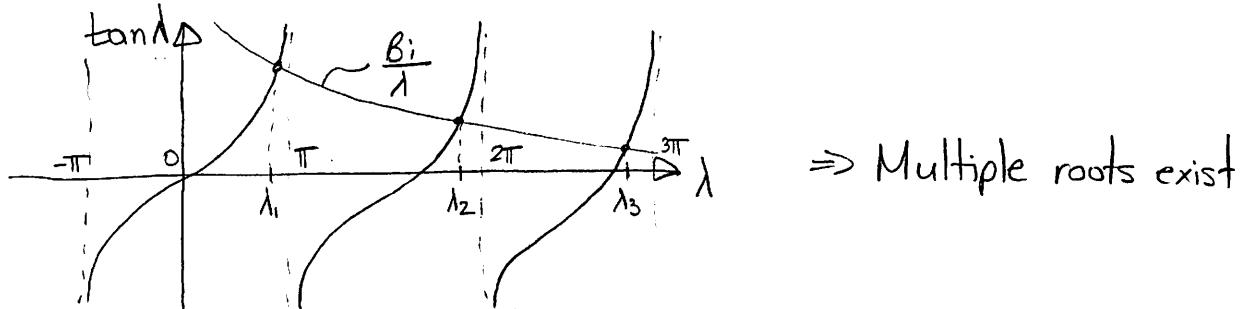
$$\frac{\partial \Theta(0, \bar{c})}{\partial \bar{x}} = 0 \Rightarrow -e^{-\lambda^2 \bar{c}} (A\lambda \sin(0) + B\lambda \cos(0)) = 0 \Rightarrow B = 0$$

$$\Theta = A e^{-\lambda^2 \bar{c}} \cos(\lambda \bar{x})$$

$$\frac{\partial \Theta(1, \bar{c})}{\partial \bar{x}} = -B_i \Theta(1, \bar{c}) \Rightarrow -A e^{-\lambda^2 \bar{c}} \lambda \sin \lambda = -B_i A e^{-\lambda^2 \bar{c}} \cos \lambda$$

$$\lambda \tan \lambda = B_i$$

We know $\tan \lambda$ is a periodic function with period π .
The solution can lie anywhere between $0 & \pi$, $\pi & 2\pi$, ...



So we have multiple solutions

$$\lambda_n \tan \lambda_n = B_i \quad (\text{Eigenfunction with eigenvalues } \lambda_n)$$

There exist an infinite number of solutions of the form $A e^{-\lambda^2 \bar{c}} \cos(\lambda \bar{x})$. The final solution is a linear combination of all of them:

$$\Theta = \sum_{n=1}^{\infty} A_n e^{-\lambda_n^2 \bar{c}} \cos(\lambda_n \bar{x})$$

Where the constants A_n are determined from our I.C.

$$\Theta(\bar{x}, 0) = 1 \rightarrow 1 = \sum_{n=1}^{\infty} A_n \cos(\lambda_n \bar{x})$$

Using orthogonality \Rightarrow multiply both sides by $\cos(\lambda_m \bar{x})$ & integrate

$$\int_0^1 \cos(\lambda_m \bar{x}) d\bar{x} = \sum_{n=1}^{\infty} A_n \underbrace{\int_0^1 \cos(\lambda_n \bar{x}) \cos(\lambda_m \bar{x}) d\bar{x}}_{=0 \text{ if } n \neq m}$$

So our solution becomes

$$\int_0^1 \cos(\lambda_n \bar{x}) d\bar{x} = A_n \int_0^1 \cos^2(\lambda_n \bar{x}) d\bar{x}$$

$$A_n = \frac{4 \sin \lambda_n}{2\lambda_n + \sin(2\lambda_n)}$$

→ Constants in the θ solution series

So now what? We can do the same for a cylinder & sphere.

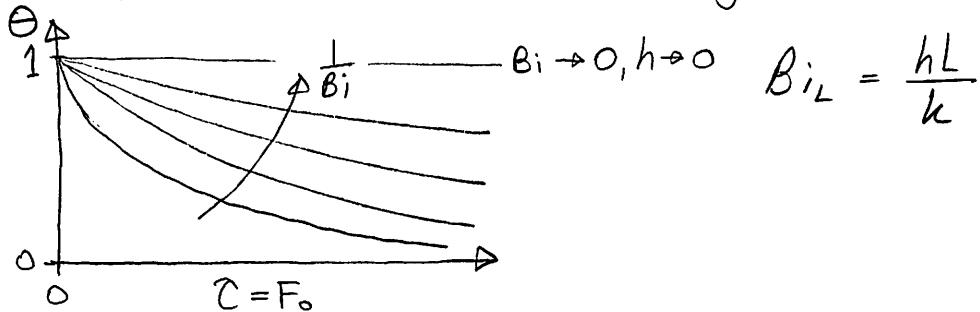
Since solution involves an infinite series, not very usefull to solve analytically. However, good approximation is made with the first few terms since rest decay rapidly due to the $e^{-\lambda_n^2 C}$ term.

END OF LECTURE 8

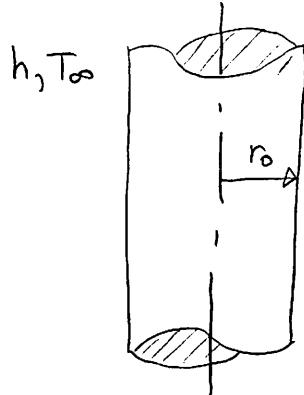
Tabular Solutions

We know our solution is: $\theta = f(\bar{x}, Bi, F_o)$

We can plot our results as: (for a given \bar{x})



Similar if we had a cylinder:

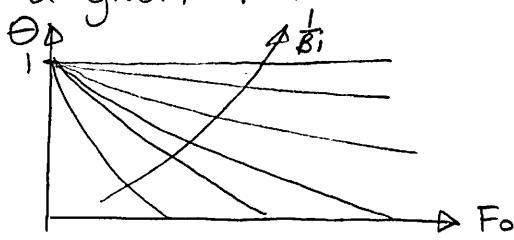


h, T_∞

$$\bar{r} = \frac{r}{r_0}, \quad \theta = f(\bar{r}, Bi_{r_0}, F_o)$$

$$Bi = \frac{hr_0}{k}$$

For a given \bar{r} :



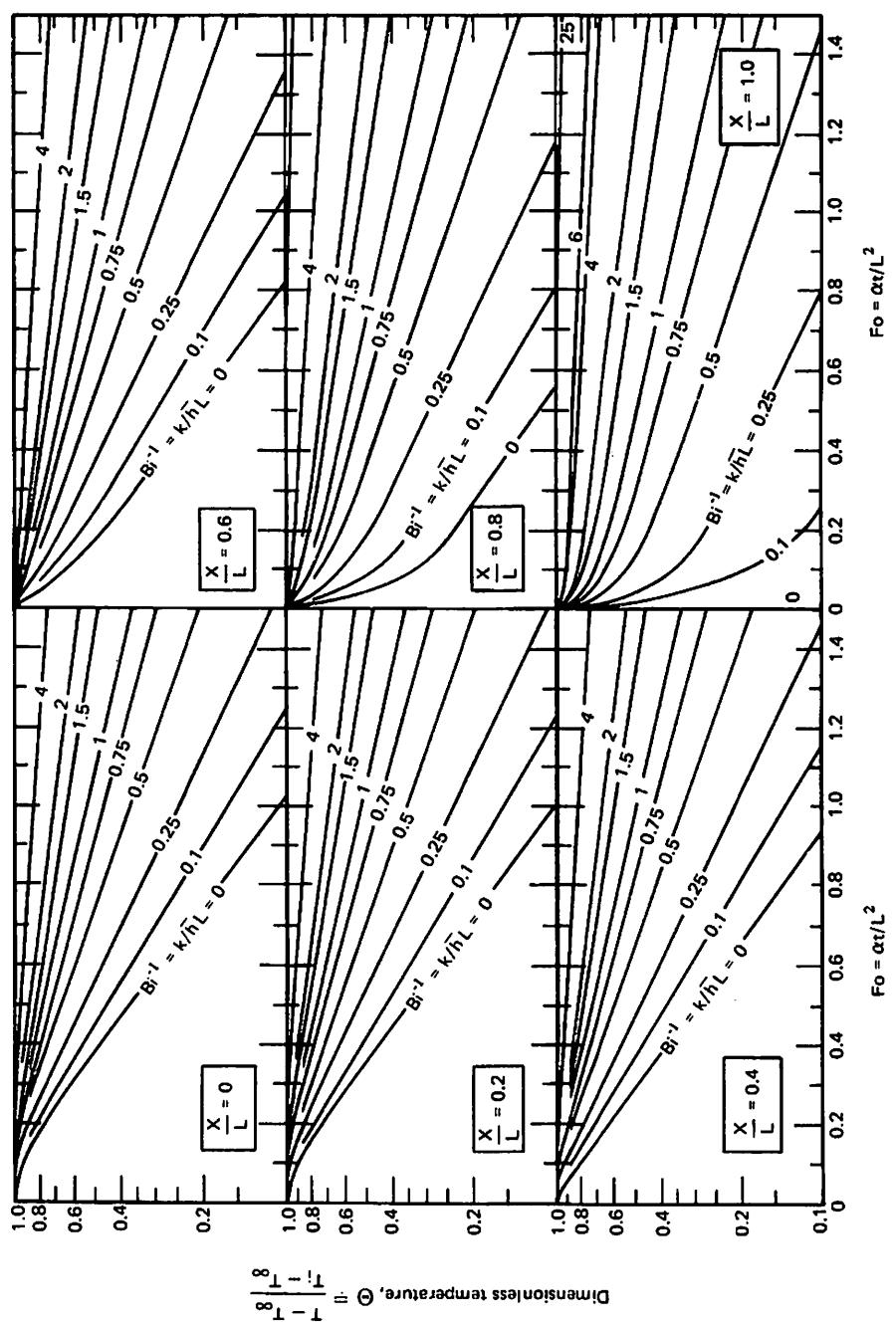


Figure 5.7 The transient temperature distribution in a slab at six positions: $x/L = 0$ is the center, $x/L = 1$ is one outside boundary.

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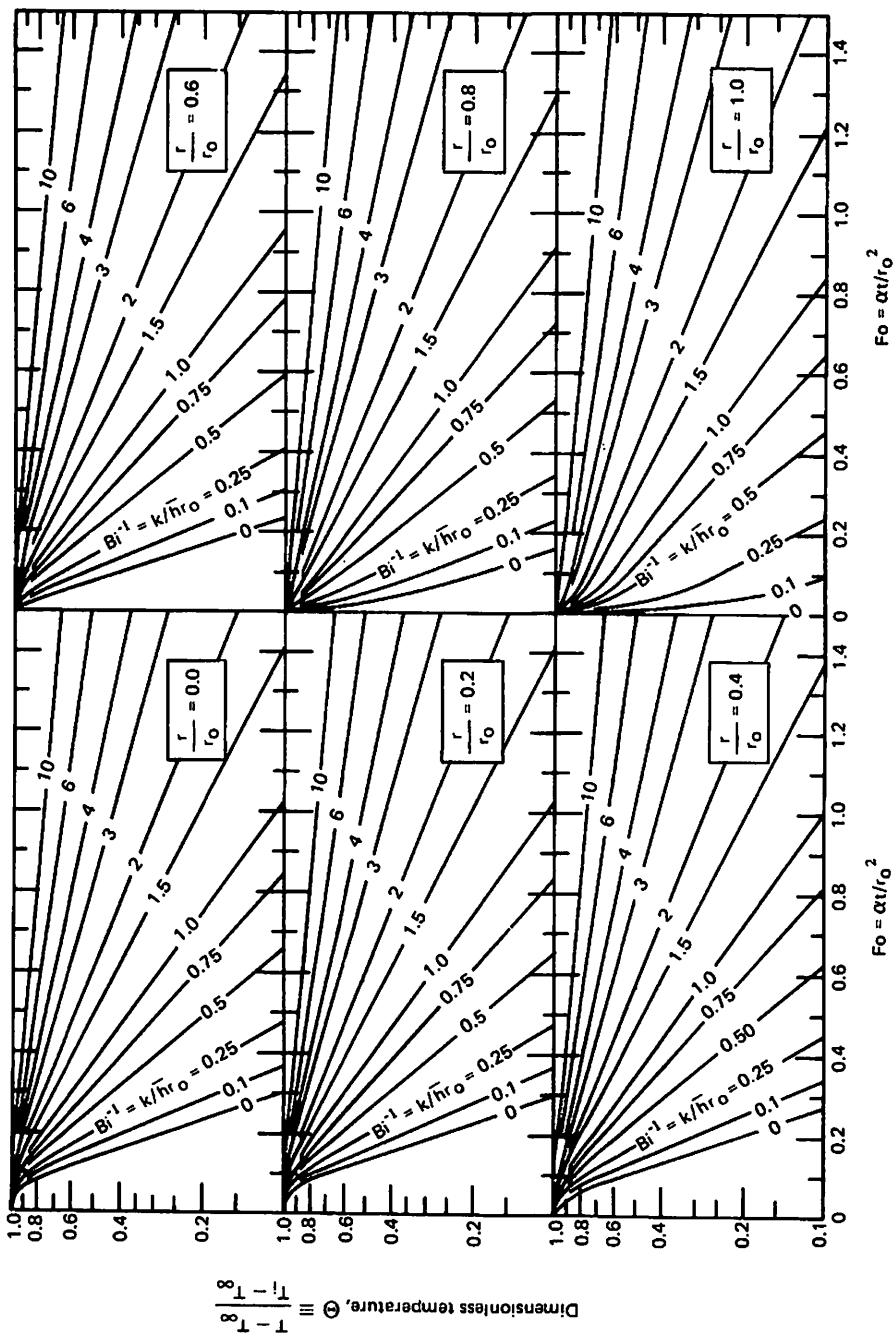


Figure 5.9 The transient temperature distribution in a sphere of radius r_o at six positions: $r/r_o = 0$ is the center; $r/r_o = 1$ is the outside boundary.

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