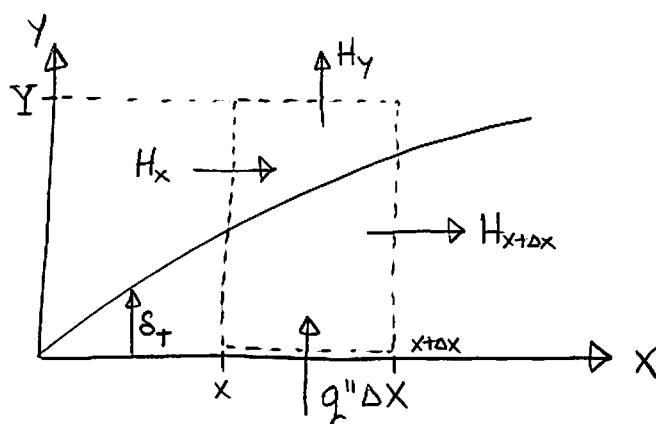


Energy Integral (Heat Transfer)

Similar to what we just did, we can develop an energy balance on our CV:



* Assuming viscous dissipation heating is negligible.

H_x = enthalpy flow in the x plane

Writing out our terms:

$$H_x = \left(\int_0^Y \rho c_p u T dy \right) \Big|_x \quad \text{Taylor Series Expans.}$$

$$H_{x+dx} = \left(\int_0^Y \rho c_p u T dy \right) \Big|_{x+dx} = \left(\int_0^Y \rho c_p u T dy \right) \Big|_x + \frac{\partial}{\partial x} \left(\int_0^Y \rho c_p u T dy \right) dx + \dots$$

$$H_y = (\rho v c_p T) \Big|_y \cdot \Delta x$$

$$q'' \Delta x = -k \frac{\partial T}{\partial y} \Big|_y \cdot \Delta x$$

Substituting all of our terms into our energy equation

$$-H_{x+dx} + H_x - H_y + q'' \Delta x = 0 \quad \text{or} \quad H_{x+dx} - H_x + H_y = q'' \Delta x$$

$$\left[\left(\int_0^Y \rho c_p u T dy \right) \Big|_x + \frac{\partial}{\partial x} \left(\int_0^Y \rho c_p u T dy \right) \Big|_x \Delta x + H.O.T \right] - \left(\int_0^Y \rho c_p u T dy \right) \Big|_x$$

$$+ (\rho v c_p T) \Big|_y \cdot \Delta x = -k \frac{\partial T}{\partial y} \Big|_y \cdot \Delta x \quad \Rightarrow \text{Divide through by } \Delta x \text{ and let } \Delta x \rightarrow 0.$$

From continuity (solved during momentum integral calculation)

$$v|_y = -\frac{\partial}{\partial x} \int_0^y u dy \Rightarrow \text{Back substitute into our } M_y \text{ term:}$$

I assumed here $\rho C_p = \text{constants}$

$$M_y = \left(\rho v C_p T \right) \Big|_y \cdot \Delta x = - \left(\rho C_p \frac{\partial}{\partial x} \int_0^y u dy \cdot T \right) \Big|_y \cdot \Delta x$$

$$M_y = - \left[\rho C_p \frac{\partial T}{\partial x} \Big|_y \int_0^y u dy + \rho C_p T \Big|_y \int_0^y \frac{\partial u}{\partial x} dy \right] \cdot \Delta x$$

Back substituting (dropping the Δx since we already canceled it).

$$\begin{aligned} \frac{\partial}{\partial x} \left(\int_0^y \rho C_p u T dy \right) \Big|_x &= \rho C_p T \Big|_y \frac{\partial}{\partial x} \int_0^y u dy - \rho C_p \frac{\partial T}{\partial x} \Big|_y \int_0^y u dy \\ &= -k \frac{\partial T}{\partial y} \Big|_y. \end{aligned}$$

Assuming $\rho C_p = \text{constant}$, & knowing $\alpha = \frac{k}{\rho C_p}$

$$\boxed{\frac{\partial}{\partial x} \int_0^y u (T_\infty - T) dy = \alpha \frac{\partial T}{\partial y} \Big|_y - \frac{\partial T}{\partial x} \int_0^y u dy}$$

↳ Integral Boundary Layer Equation for Energy

Usually, we assume two things to simplify:

- 1) Integrate to $y = S_T$ since for $y > S_T \Rightarrow$ integrals become 0.
- 2) The $T_\infty = \text{constant}$. For the above equation, it doesn't need to be however.

$$\boxed{\frac{\partial}{\partial x} \int_0^y u (T_\infty - T) dy = \alpha \frac{\partial T}{\partial y} \Big|_y} \Rightarrow T_\infty = \text{constant}$$

①

So let's try the same approach we used for the momentum integral:

$$\Theta(\eta_T) = \frac{T - T_0}{T_\infty - T_0} ; \quad \eta_T = \frac{y}{S_T} \Rightarrow d\theta = (T_\infty - T_0) dT \\ dy = S_T d\eta_T$$

We see right away that:

$$\frac{T - T_\infty}{T_0 - T_\infty} = 1 - \frac{T - T_0}{T_\infty - T_0} = 1 - \Theta$$

Back substituting into ① \Rightarrow Also $\phi = \frac{U}{U_\infty}$

$$\frac{2}{2x} \int_0^1 U_\infty \phi (1-\Theta) (T_0 - T_\infty) S_T d\eta_T = \left. \frac{\alpha}{S_T} \frac{\partial \Theta}{\partial \eta_T} \right|_0 \cdot (T_0 - T_\infty)$$

$$\frac{2}{2x} \int_0^1 S_T \phi (1-\Theta) \partial \eta_T = \left. \frac{\alpha}{U_\infty S_T} \frac{\partial \Theta}{\partial \eta_T} \right|_0 \quad ②$$

Our B.C.'s are:

$$\Theta(\eta_T=0) = 0 \quad (\text{Wall temperature, } T_0)$$

$$\Theta(\eta_T=1) = 1 \quad (\text{Free stream temperature, } T_\infty)$$

$$\Theta'(\eta_T=1) = 0 \quad (\text{No temp. gradient at b.l. edge})$$

$$\Theta''(\eta_T=0) = 0 \quad (\text{Linear Temp. profile at wall})$$

Using the identical clever math trick as before:

$$\Theta(\eta^*) = \frac{S}{S_T} \phi ; \quad \eta^* = \eta \Pr^{1/3}$$

We can check the rationality of our assumption

$$\left[\phi = \frac{3}{2} \eta - \frac{1}{2} \eta^3 = \frac{3}{2} \cdot \frac{y}{S} - \frac{1}{2} \left(\frac{y}{S} \right)^3 \right] \cdot \frac{S}{S_T}$$

$$\Theta = \frac{3}{2} \left(\frac{y}{S_T} \right) - \frac{1}{2} \left(\frac{y^3}{S^2 S_T} \right) \Rightarrow \text{Note here we can simplify}$$

We've implicitly assumed that $U \propto U_\infty$, i.e. $Pr \approx 1$ or $Pr \gg 1$. Because of this assumption, we can safely say that $\delta > \delta_T$. So comparing our two terms near the wall (where it's important)

$$\frac{\frac{3}{2} \left(\frac{y}{\delta_T} \right)}{\frac{1}{2} \left(\frac{y^3}{\delta^2 \delta_T} \right)} = \frac{3\delta^2}{y^2} \gg 1 \Rightarrow \text{Since for energy solution } (\theta) \\ 0 < y < \delta_T, y_{\max} = \delta_T \\ = \frac{3\delta^2}{\delta_T^2} \gg 1 \text{ since } Pr \approx 1 \text{ or } Pr \gg 1$$

So this allows us to safely say that the second term in our θ solution is negligible compared to the first.

Note, this is also possible because our B.C.'s in non-dimensional momentum (ϕ) and energy (θ) are identical.

Now we have the following:

$$\theta(n^*) = \frac{3}{2} \frac{y}{\delta_T} \Rightarrow \text{Back substitute into } ② \quad \left(\phi = \frac{\delta_T}{\delta} \theta \right)$$

$$\frac{2}{\partial x} \left(\frac{\delta_T^2}{\delta} \right) \int_0^1 \theta(1-\theta) d\eta_T = \frac{\alpha}{U \delta_T} \left(\frac{U}{U_\infty} \theta' \Big|_0 \right)$$

$$\frac{2}{\partial x} \left(\frac{\delta_T^2}{\delta} \right) = \frac{1}{Pr \delta_T} \cdot \frac{U}{U_\infty} \underbrace{\left[\frac{\theta' \Big|_0}{\int_0^1 \theta(1-\theta) d\eta_T} \right]}_{\beta}$$

Rearranging:

$\beta \Rightarrow$ We've defined this before!

$$\delta_T \frac{2}{\partial x} \left(\frac{\delta_T^2}{\delta} \right) = \underbrace{\frac{1}{Pr} \left(\frac{U}{U_\infty} \beta \right)}_{= \delta \frac{\partial \delta}{\partial x}} \quad (\text{Derived this before})$$

$$S_T \frac{\partial}{\partial x} \left(\frac{S_T^2}{S} \right) = \frac{S}{Pr} \frac{\partial S}{\partial x} \cdot \left(\frac{S''^2}{S^{1/2}} \right) \Rightarrow \text{Integrate both sides}$$

$$\int_{x_0}^x \frac{S_T}{S^{1/2}} \frac{\partial}{\partial x} \left(\frac{S_T^2}{S} \right) = \int_{x_0}^x \frac{1}{Pr} S^{1/2} \frac{\partial S}{\partial x} \Rightarrow \text{Note, my bounds of integration are } x_0 \text{ to } x. \\ I \text{ will explain later!}$$

$$\Rightarrow \underbrace{\int_{x_0}^x \frac{S_T}{S^{3/2}} d(S_T^2)}_{= \int_{x_0}^x \frac{1}{Pr} S^{1/2} dS}$$

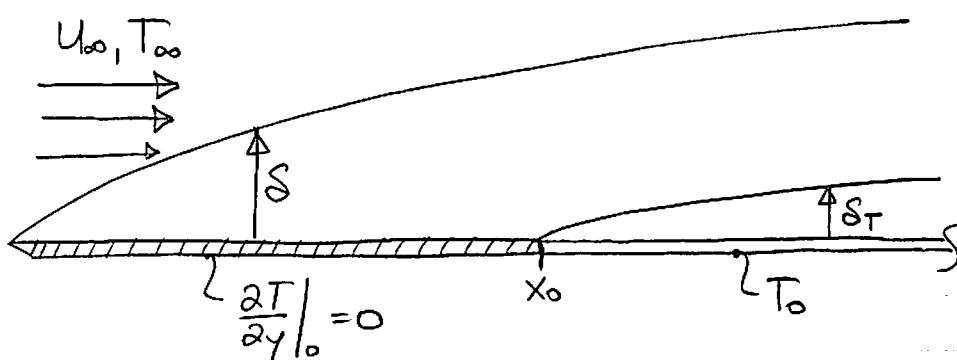
$$\int_{x_0}^x \frac{S_T}{S^{3/2}} 2S_T dS_T = \int_{x_0}^x \frac{2S_T^2}{S^{3/2}} dS_T = \frac{2}{3} \frac{S_T^3}{S^{3/2}} \Big|_{x_0}^x$$

Our second integral is more trivial : $\int_{x_0}^x S^{1/2} dS = \frac{2}{3} S^{3/2} \Big|_{x_0}^x$

$$\frac{2}{3} \frac{S_T^3}{S^{3/2}} \Big|_{x_0}^x = \frac{2}{3} S^{3/2} \Big|_{x_0}^x$$

$$\left(\frac{S_T^2}{S} \right)^{3/2} = \frac{1}{Pr} S^{3/2} \left[1 - \left(\frac{S_0}{S} \right)^{3/2} \right]$$

So the reason we integrated from x_0 instead of 0 is because it allows us to get a much more general and powerful solution. The physical picture is the following:



So for this situation, at x_0 , $S_T = 0$ and $S_0 = C\sqrt{x}$.

Note: $\frac{S}{x} \sim \frac{C}{Re_x^{1/2}} \Rightarrow S \sim \sqrt{x}$

$$\left(\frac{\delta_T}{\delta}\right)^3 = \frac{1}{Pr} \left(1 - \left(\frac{x_0}{x}\right)^{3/4}\right) \Rightarrow I \text{ subbed in } S_0 = C\sqrt{x_0} \text{ & } \delta = C\sqrt{x}$$

$$\boxed{\frac{\delta}{\delta_T} = Pr^{1/3} \cdot \left[1 - \left(\frac{x_0}{x}\right)^{3/4}\right]^{-1/3}}$$

\Rightarrow Note, we didn't assume a Θ profile and got this! Only assumed $\delta \sim \sqrt{x}$ which is obvious!

Note, if we check our result with $x_0 = 0$, we obtain the same familiar result as before:

$$\boxed{\frac{\delta}{\delta_T} = Pr^{1/3}} \Rightarrow x_0 = 0, Pr \geq 1.$$

So how do we calculate heat transfer?

$$q'' \Big|_{y=0} = -k \frac{\partial T}{\partial y} \Big|_0 = -\frac{k}{\delta_T} \cdot \frac{\partial \Theta}{\partial n_T} \cdot \underbrace{(T_\infty - T_0)}_{-\Delta T} \Rightarrow \text{Remember from before:}$$

$$\partial \Theta = (T_\infty - T_0) \partial T$$

$$2y = \delta_T \partial n_T$$

For $x > x_0$

$$q'' \Big|_{y=0} = \frac{k \Delta T}{\delta_T} \Theta' \Big|_0 = \frac{k \Delta T}{x} \frac{\Theta' \Big|_0}{\left(\frac{\delta_T}{\delta}\right) \left(\frac{\delta}{x}\right)}$$

We know that:

$$\frac{\delta_T}{\delta} = Pr^{-1/3} \left[1 - \left(\frac{x_0}{x}\right)^{3/4}\right]^{1/3} \quad \text{and} \quad \frac{\delta}{x} = \frac{\sqrt{2\beta}}{Re_x^{1/2}} \Rightarrow \text{Back substitute:}$$

$$q'' \Big|_{y=0} = \left(\frac{k \Delta T}{x}\right) \frac{Pr^{1/3} Re_x^{1/2} \Theta' \Big|_0}{\left[1 - \left(\frac{x_0}{x}\right)^{3/4}\right]^{1/3} \sqrt{2\beta}} \Rightarrow \text{Expand this by substituting } \beta$$

$$\boxed{q'' \Big|_{y=0} = \left(\frac{k \Delta T}{x}\right) \left[\frac{\Theta' \Big|_0}{2} \int_0^1 \Theta(1-\Theta) d n_T \right]^{1/2} \cdot \frac{Re_x^{1/2} Pr^{1/3}}{\left[1 - \left(\frac{x_0}{x}\right)^{3/4}\right]^{1/3}}}$$

To solve, we need to assume a temperature profile $\Theta(n_T)$.

However there is something nice we can use about this solution and our previous similarity solutions:

$$\left[\frac{\Theta'|_0}{2} \int_0^1 \Theta(1-\Theta) d\eta_T \right]^{1/2} \neq f(x_0)$$

We know that in our limit of $x_0 = 0$, this term must be 0.332 (similarity solution). Hence:

$$\boxed{\left[\frac{\Theta'|_0}{2} \int_0^1 \Theta(1-\Theta) d\eta_T \right]^{1/2} = 0.332} \Rightarrow \text{Try it for a few profiles.}$$

Let's see how good we are. We already assumed before:

$$\Theta = \frac{3}{2} \eta_T - \frac{1}{2} \eta_T^3$$

$$\Theta'|_0 = \frac{3}{2}$$

$$\begin{aligned} \int_0^1 \Theta(1-\Theta) d\eta_T &= \int_0^1 \left(\frac{3}{2} \eta_T - \frac{1}{2} \eta_T^3 \right) \left(1 - \frac{3}{2} \eta_T + \frac{1}{2} \eta_T^3 \right) d\eta_T \\ &= \int_0^1 \left(\frac{3}{2} \eta_T - \frac{9}{4} \eta_T^2 + \frac{1}{3} \eta_T^3 + \frac{3}{2} \eta_T^4 - \frac{1}{4} \eta_T^6 \right) d\eta_T \\ &= \left[\frac{3}{4} - \frac{9}{12} + \frac{3}{10} - \frac{1}{8} - \frac{1}{28} \right] = 0.13928 \end{aligned}$$

$$\left[\frac{\Theta'|_0}{2} \int_0^1 \Theta(1-\Theta) d\eta_T \right]^{1/2} = \left[\frac{3}{4} \left(\frac{3}{10} - \frac{1}{8} - \frac{1}{28} \right) \right]^{1/2} = 0.3232$$

So with $\Theta = \frac{3}{2} \eta_T - \frac{1}{2} \eta_T^3 \Rightarrow$ Our constant is 0.3232!

So finally, our solution becomes:

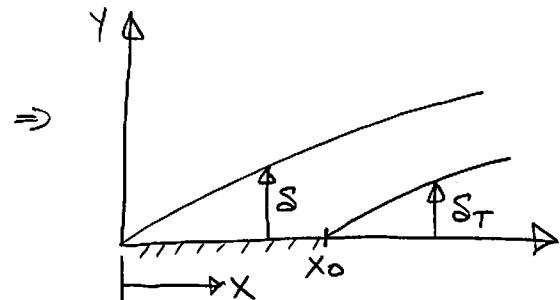
$$q''|_{y=0} = 0.332 \frac{k\Delta T}{x} \cdot \frac{Re^{1/2} Pr^{1/3}}{\left[1 - \left(\frac{x_0}{x}\right)^{3/4}\right]^{1/3}}$$

$$h = \frac{q''|_{y=0}}{\Delta T} = \frac{0.332k}{x} \dots$$

$$Nu_x = 0.332 \frac{Re^{1/2} Pr^{1/2}}{\left[1 - \left(\frac{x_0}{x}\right)^{3/4}\right]^{1/3}} \Rightarrow \text{Laminar}$$

$$\Rightarrow \text{From } Nu_x = \frac{hx}{k} = \frac{q''|_0}{\Delta T} \cdot \frac{x}{k}$$

$$\Rightarrow U_\infty, \Delta T = \text{const.}$$

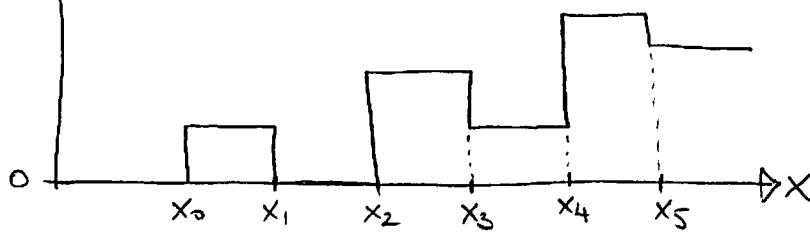


Our result kind of makes sense, however be careful. It is valid for $x > x_0$. For $x < x_0$, we've defined the plate to be adiabatic, so our solution gives us non-physical answers.

Arbitrary Varying Temperature Difference

What if instead of just one simple temperature jump like above, we had an arbitrarily varying wall temperature with multiple jumps?

$$(T_0 - T_\infty)$$



Looking at our energy equation again reveals the solution:

$$U \frac{\partial T}{\partial x} + V \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2} \Rightarrow \text{Linear Differential Equation}$$

We can use Duhamel's Theorem to say that superposition of any number of stepwise variations is a valid solution.

What Duhamel's Theorem implies is the following:

$$T = \sum_i^n T_i \Rightarrow T_i = \text{a particular solution to the energy equation for specific boundary cond.}$$

Try substituting this in, you will see that it works out.

At the surface, we know:

$$q''|_o = -k \frac{\partial T}{\partial y}|_o = -k \sum_i^n \frac{\partial T_i}{\partial y}|_o$$

Here, we can invoke that each particular solution corresponds to a temperature jump ΔT_i . For each particular solution, we can say:

$$-k \frac{\partial T_i}{\partial y}|_o = h_i \Delta T_i$$

Hence, for the full solution, we can say:

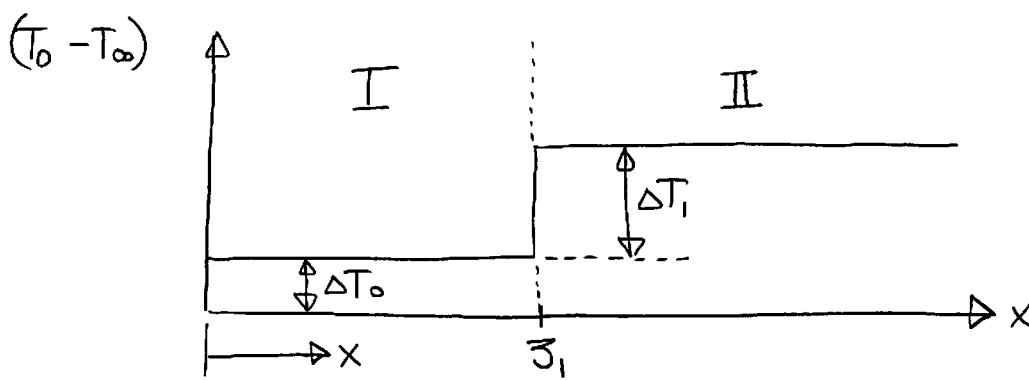
$$q'' = \sum_i^n h_i \Delta T_i$$

Translating this to our previous solution, we say:

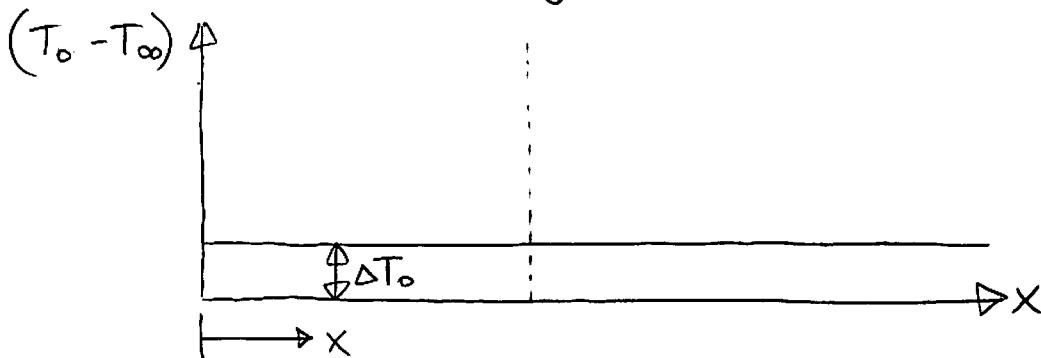
$$q'' = \sum_i^n h(x, x_{o,i}) \Delta T_i \quad ①$$

h = heat transfer coefficient which describes heat flow at location x when only one step ΔT_i in the wall temperature occurs at location $x_{o,i}$.

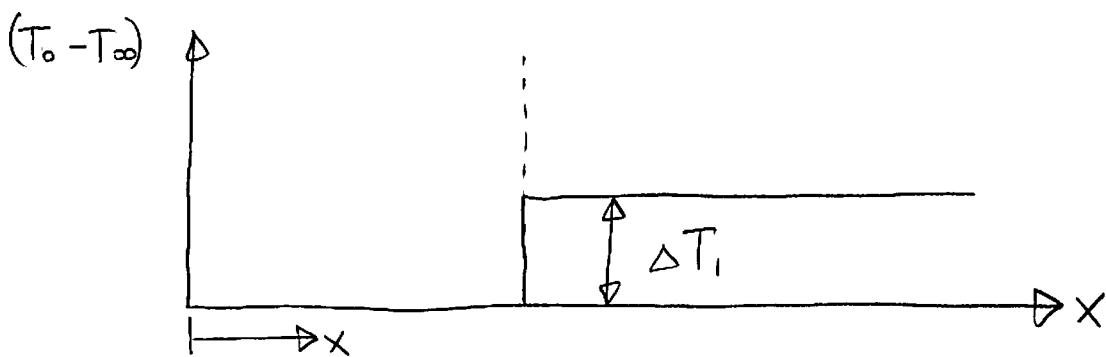
Note, this method of solution (superposition) can also be applied to other linear ODEs & PDEs, (i.e., wave equation).



↔ Equivalent to



+



In general, we can say:

$$(T - T_{\infty}) = \sum_{j=0}^n \Delta T_j \cdot f(x, y, z_j) \quad ; \quad z_n < x < z_{n+1}$$

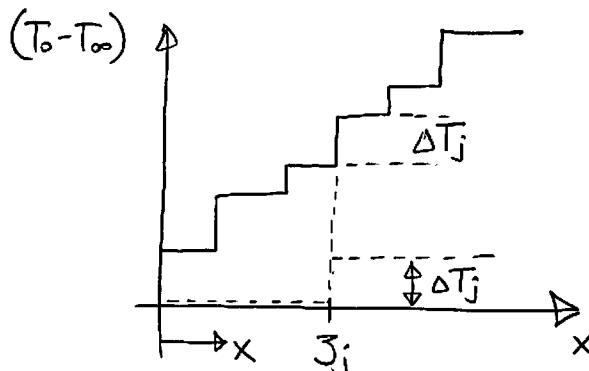
$$(T - T_{\infty}) = (T_0 - T_{\infty}) f(x, y, z)$$

Similarly: (from equation ① on the previous page)

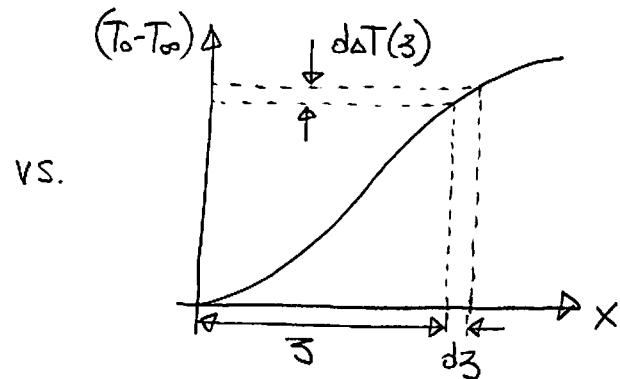
$$q''|_0 = 0.332 \left(\frac{k}{x} \right) Re_x^{1/2} Pr^{1/3} \sum_{j=0}^n \frac{\Delta T_j}{\left[1 - \left(\frac{z_j}{x} \right)^{3/4} \right]^{1/3}} \quad ; \quad z_n < x < z_{n+1}$$

↳ $U_{\infty} = \text{constant}$; Laminar; $\Delta T_j = \text{constant}$

This is valid for a stepwise variation in wall temperature. What if the variation is continuous?



Stepwise (Eq. ②)



Continuous

For the continuous case, we can change ① to:

$$q''|_o = \int_0^x h(x, z) d\Delta T(z)$$

To represent this integral in terms of our independent variable, z , we use:

$$d\Delta T(z) = \frac{d\Delta T(z)}{dz} \cdot dz$$

$$q''|_o = \int_0^x h(x, z) \frac{d\Delta T(z)}{dz} dz$$

Or in our notation: $\frac{d\Delta T(z)}{dz} = \frac{d(T_w - T_\infty)}{dz}$

$$q''|_o = 0.332 \left(\frac{k}{x} \right) Re_x^{1/2} Pr^{1/3} \int_0^x \frac{\frac{d(T_w - T_\infty)}{dz}}{\left[1 - \left(\frac{z}{x} \right)^{3/4} \right]^{1/3}} dz$$

↳ Laminar; $U_\infty = \text{constant}$; Continuous temperature difference variation.